



7<sup>th</sup> May, 2003

# Controlling Fossil Power Plant CO<sub>2</sub> Emissions

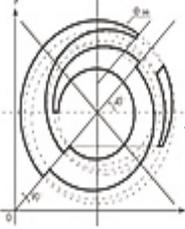
Near Term and Long Range Views

Carl Bozzuto

VP Technology, Power Environment Sector

**ALSTOM**

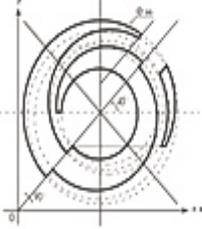
- Fossil Fuels are the mainstay of today's economy and will be needed for a long time to come.
- Coal provides over half of the US electricity generation. Coal will be needed for electric generation well into the future. Coal is a domestic resource which can be stored to reduce price volatility.
- Natural gas sets the targets for emissions from power plants. Our goal is to make the other fuels comparable to gas in regard to emissions.



# Average Emission Rates - NSPS



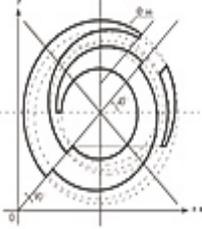
	Coal g/kwhr	Gas g/kwhr
NOx	0.7	0.2
SO2	3.0	0.003
Particulate	0.15	0.01
CO2	1000	450



# Average Emission Rates Clear Skies

**ALSTOM**

	Coal g/kwhr	Gas g/kwhr
NOx	0.2	0.06
SO2	0.3	0.003
Particulate	0.08	0.01
CO2	900	450



# Average Emission Rates Long Term

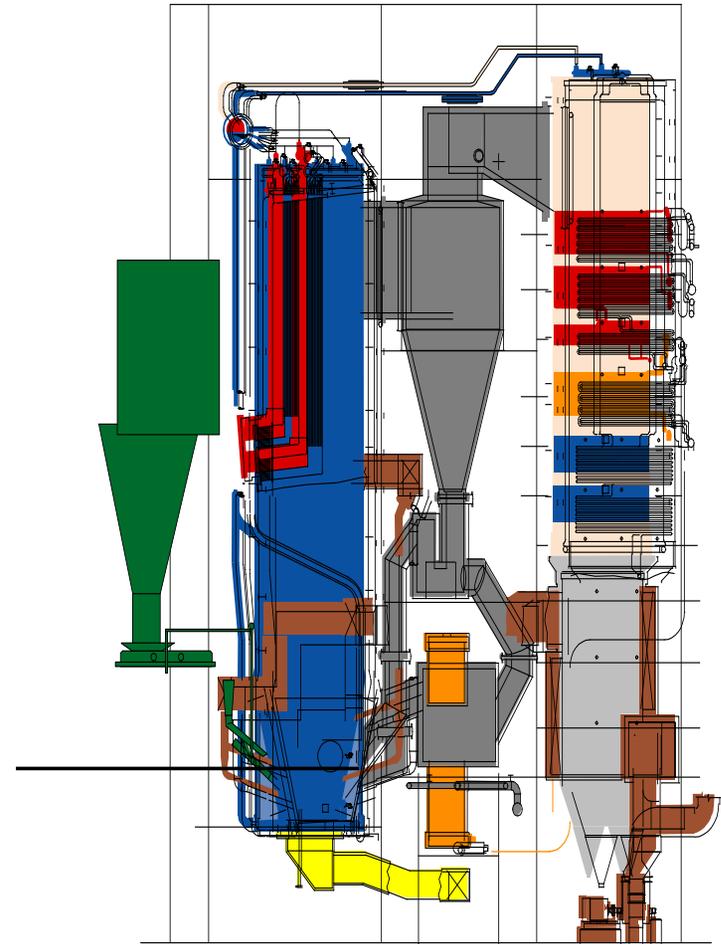


	Coal g/kwhr	Gas g/kwhr
NOx	0.05	0.03
SO2	0.03	0.003
Particulate	0.04	0.01
CO2	90	45

# Fluidized Bed Systems



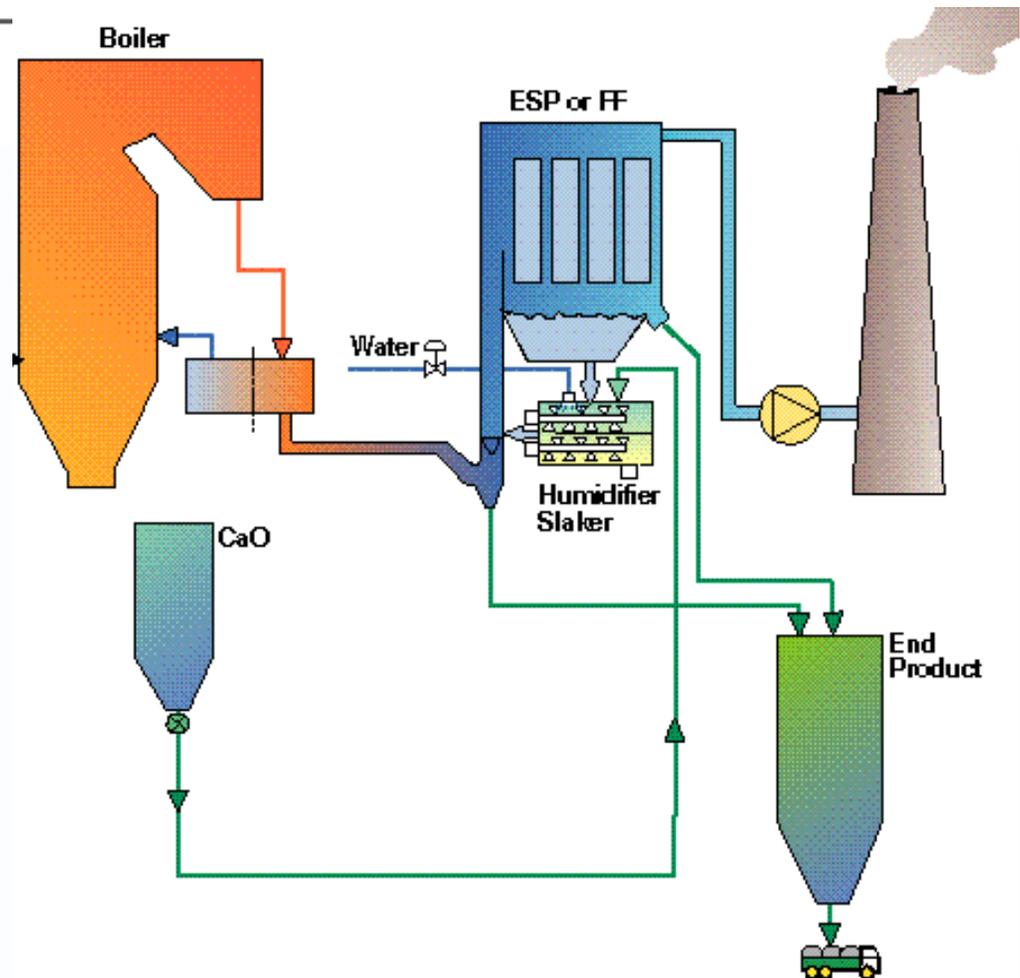
- Reduce Costs (new designs)
- Ultra Clean (integrated APC)
- Grow in Size  
(up to 600 MW USC)
- Enable Re - Powering
- Enable CO<sub>2</sub> capture from  
combustion based power  
generation



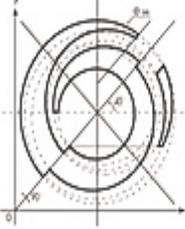
# FDA Process: Dry Injection FGD

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- § Dry Injection Process Utilizing
- § Enhanced Reagent
- § Performance equal to DFGD
- § Completed a total of 400 MW installation



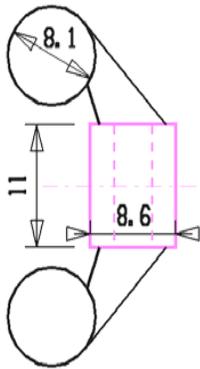
95%+ SO<sub>2</sub> Removal



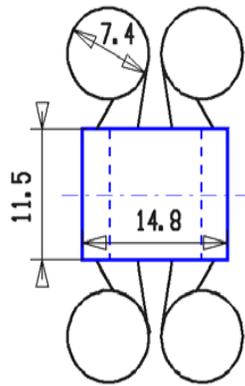
# CFB Process Scale-up :Furnace and cyclones



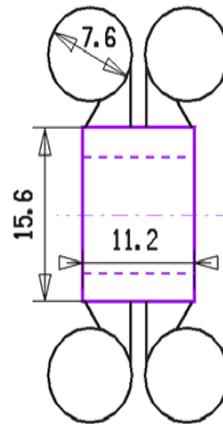
EMILE HUCHET



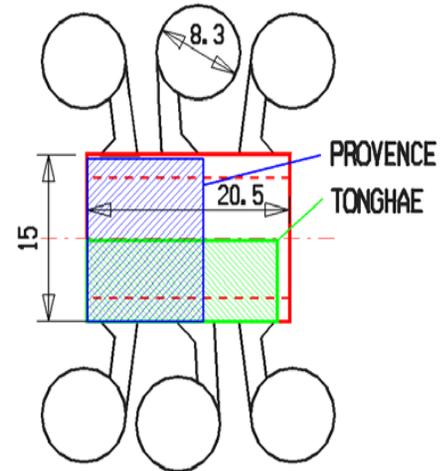
PROVENCE



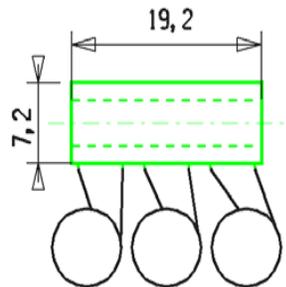
RED HILLS



APD 600 MW LFC



TONGHAE



## OBJECTIVES

Develop a CFB boiler able to compete economically with PC boilers in the range of 600 MW while taking advantage of CFB's environmental performances and flexibility.

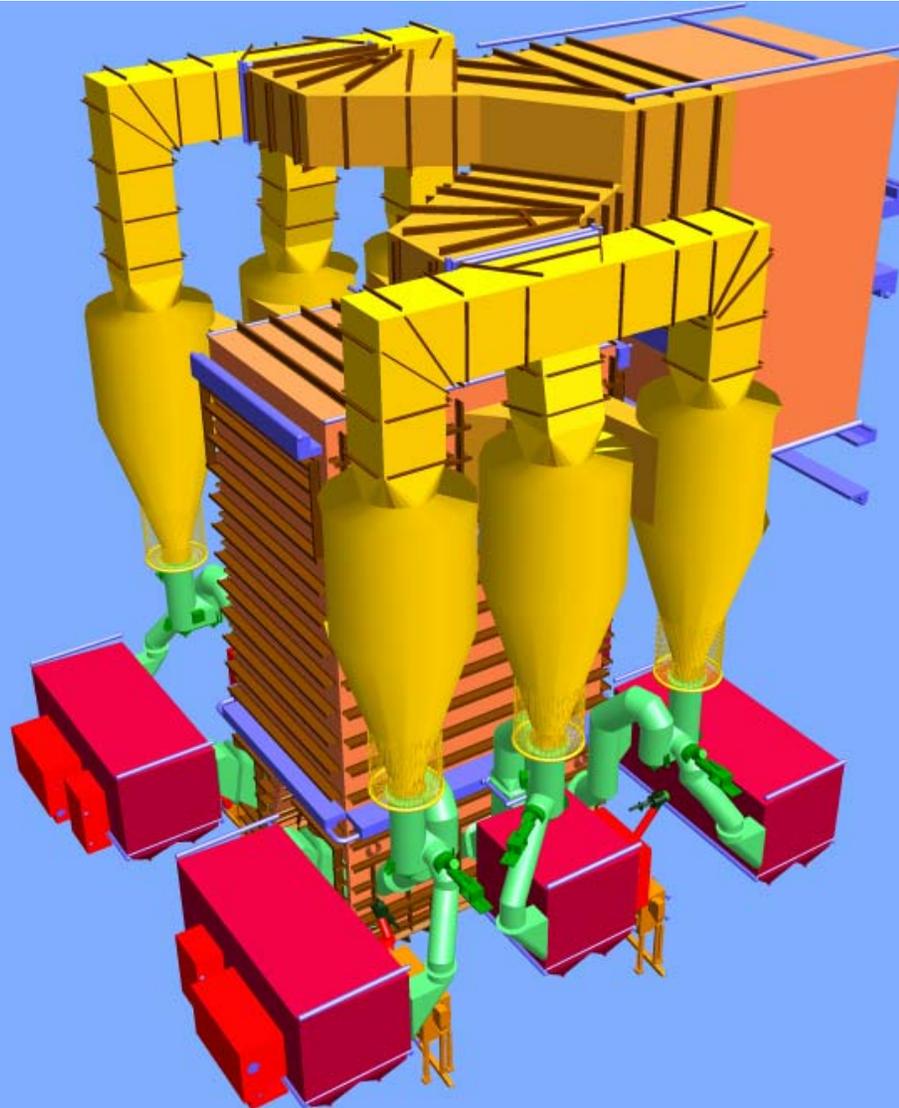
## MAIN CHALLENGES

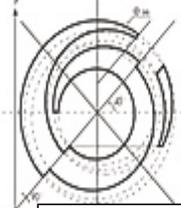
- Scale-up CFB size from existing 250 MW units up to 600 MW
- Accommodate CFB process and once through supercritical constraints:
  - tube protection against overheating
  - heat transfer surfaces distribution
- Accommodate high steam conditions: 3958 PSI/1112°F/1112°F
- Low emission levels:

SO <sub>2</sub>	200mg/Nm <sup>3</sup> (0.16 Lb/MM BTU)
NO <sub>x</sub>	200mg/Nm <sup>3</sup> (0.16 Lb/MM BTU)
CO	100mg/Nm <sup>3</sup> (0.08 Lb/MM BTU)

# 600 MW CFB BOILER General Arrangement

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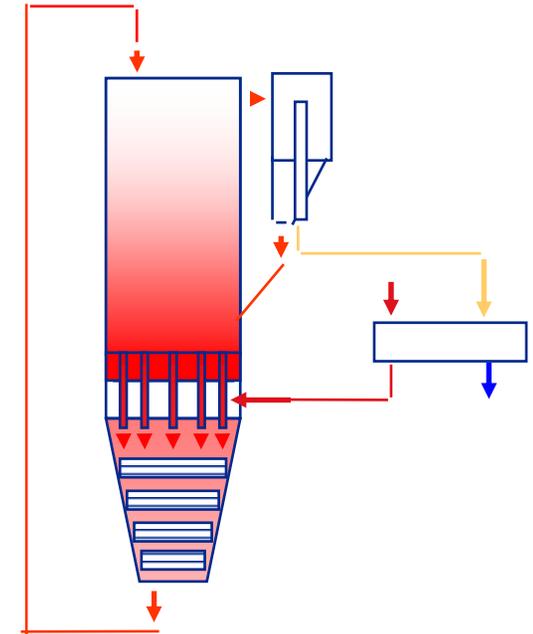


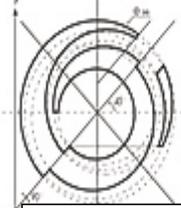


# Circulating Moving Bed

ALSTOM

- **Separate heat transfer from combustion.**
- **Potential 30% cost savings in the boiler island**
- **More effective surface allows higher steam conditions at lower cost**
- **15% Lower auxiliary power**
- **Lower emissions**
- **3 - 5 years time frame**

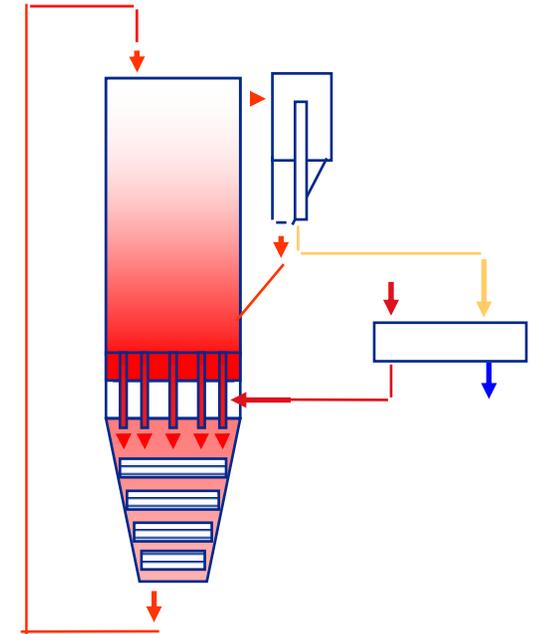




# Circulating Moving Bed

ALSTOM

- **DOE Contract for pilot testing.**
- **Heat transfer tests verify potential 30% cost savings in the boiler island**
- **High temperature tests show no evidence of plugging or sticky ash**
- **Moving bed heat exchanger demonstrated.**
- **Will need field demonstration to prove solids distribution in large units**



## 1) “Tail-end” CO<sub>2</sub> capture

- adsorption/stripping process (MEA, MEA/MDEA, physical absorbents)

## 2) Oxygen combustion

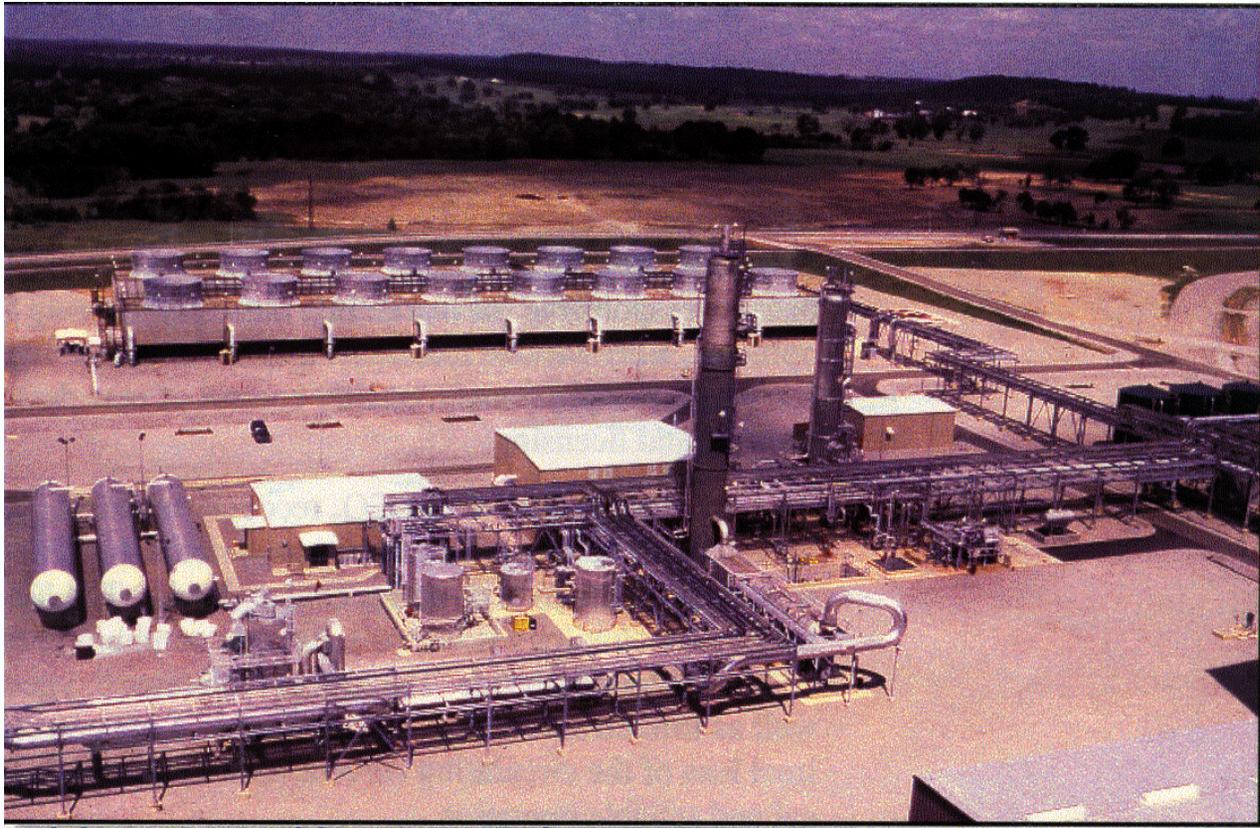
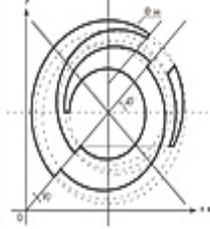
- internal (membrane) or external (ASU) O<sub>2</sub>

## 3) Other options

- oxidation/reduction cycles
- carbonate capture
- chemical looping
- syngas decarbonization

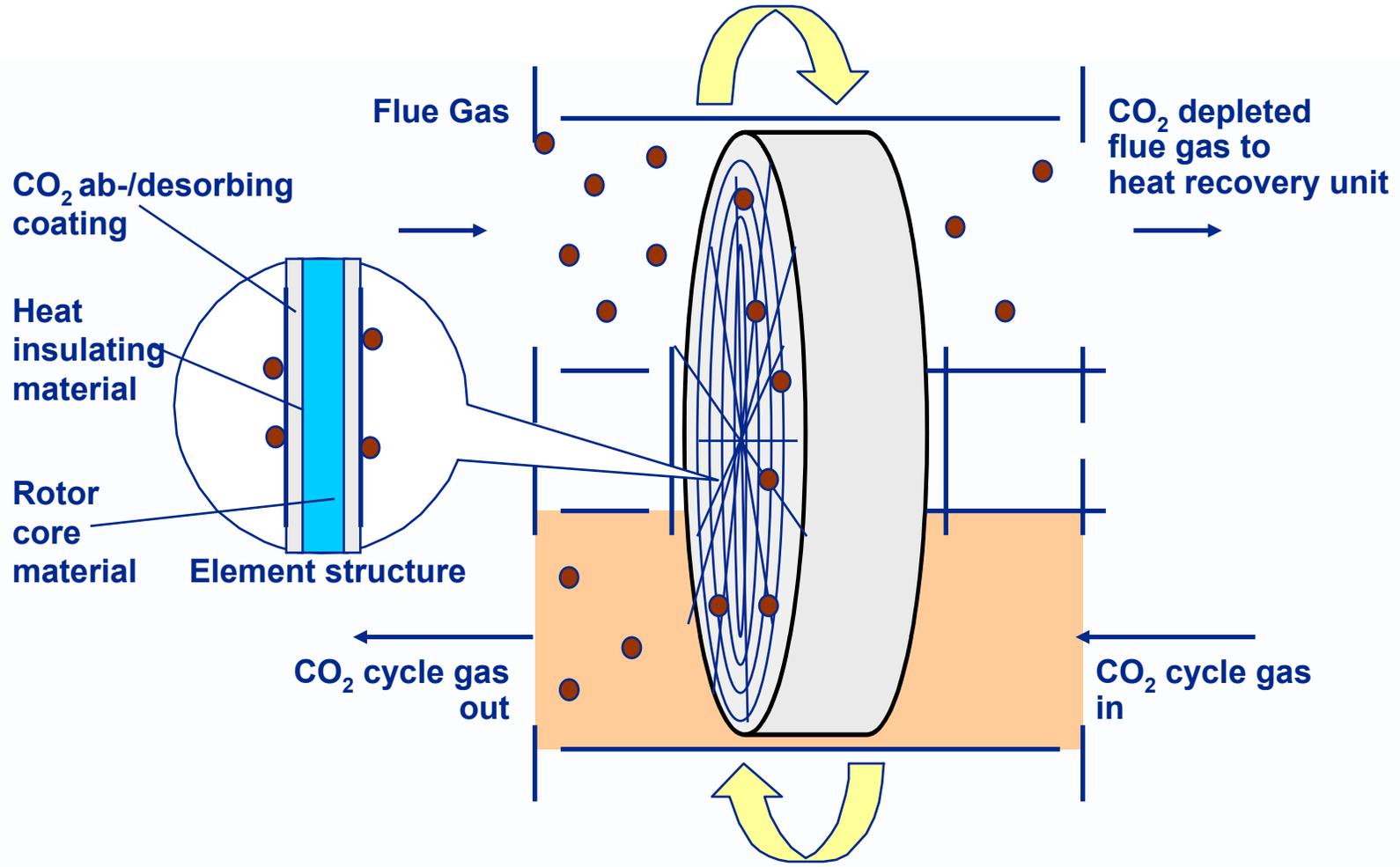


Innovative technology options just now emerging



**AES Shady Point - CO<sub>2</sub> absorber (left) and stripper (right)**

# CO<sub>2</sub> Capturing Mechanism and Element Structure

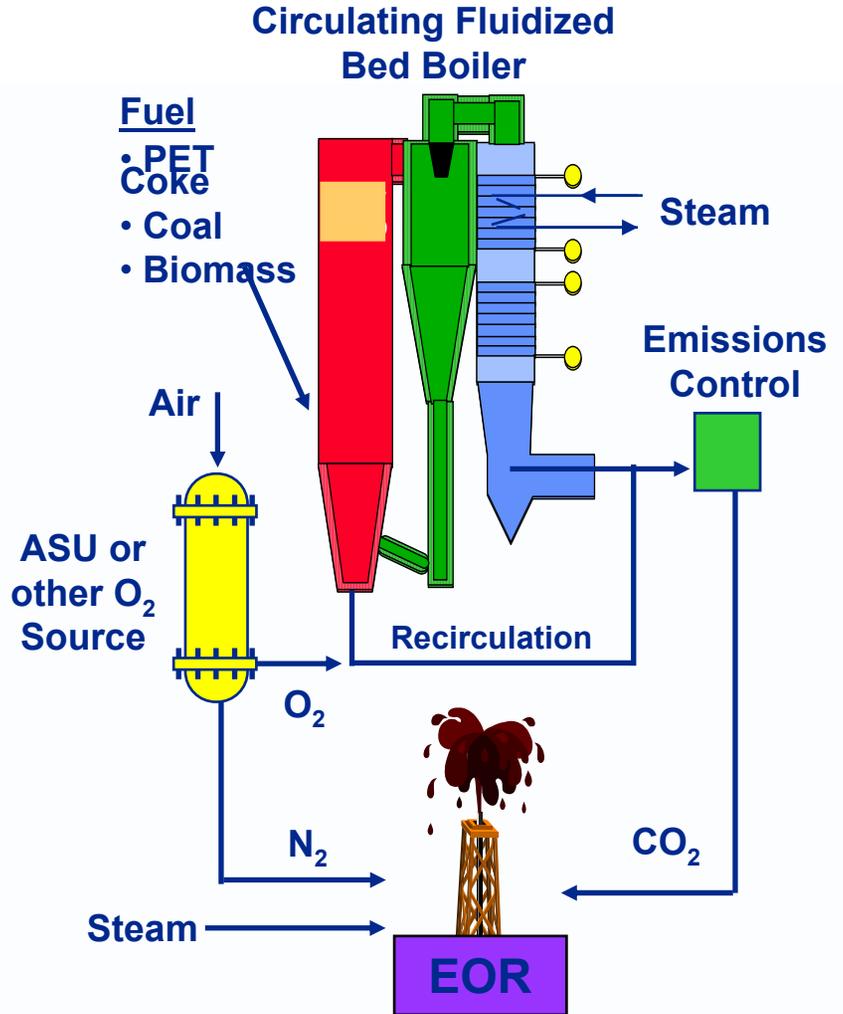


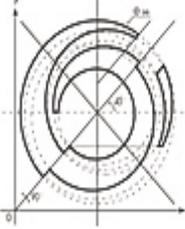
# DOE Greenhouse Gas Management Oxygen Fired CFB

## ALSTOM



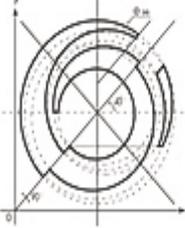
- Can use multiple fuels
  - coal, petcoke, biomass
  - opportunity fuels, tar sands
- Use circulating solids to control furnace temperature
- Retrofittable
- Opportunities to make significant size (= \$) reductions in greenfield design
- Existing/expanding market for EOR





## Advantages:

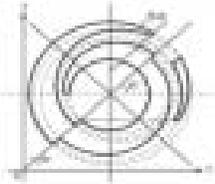
- Produces a slipstream with  $> 95\%$  CO<sub>2</sub>
- Approx 80% capture of CO<sub>2</sub>
- Air blown -- No O<sub>2</sub> feed
- No energy penalty before CO<sub>2</sub> liquefaction
- Sorbent lost to the CO<sub>2</sub> cycle is usable by FDA for SO<sub>2</sub> capture
- A CFB system could capture 30 - 40% of CO<sub>2</sub>. This could be used as a more near term solution.
  - CFB in 4 - 5 years
  - Adv.FB in 5 - 8 years



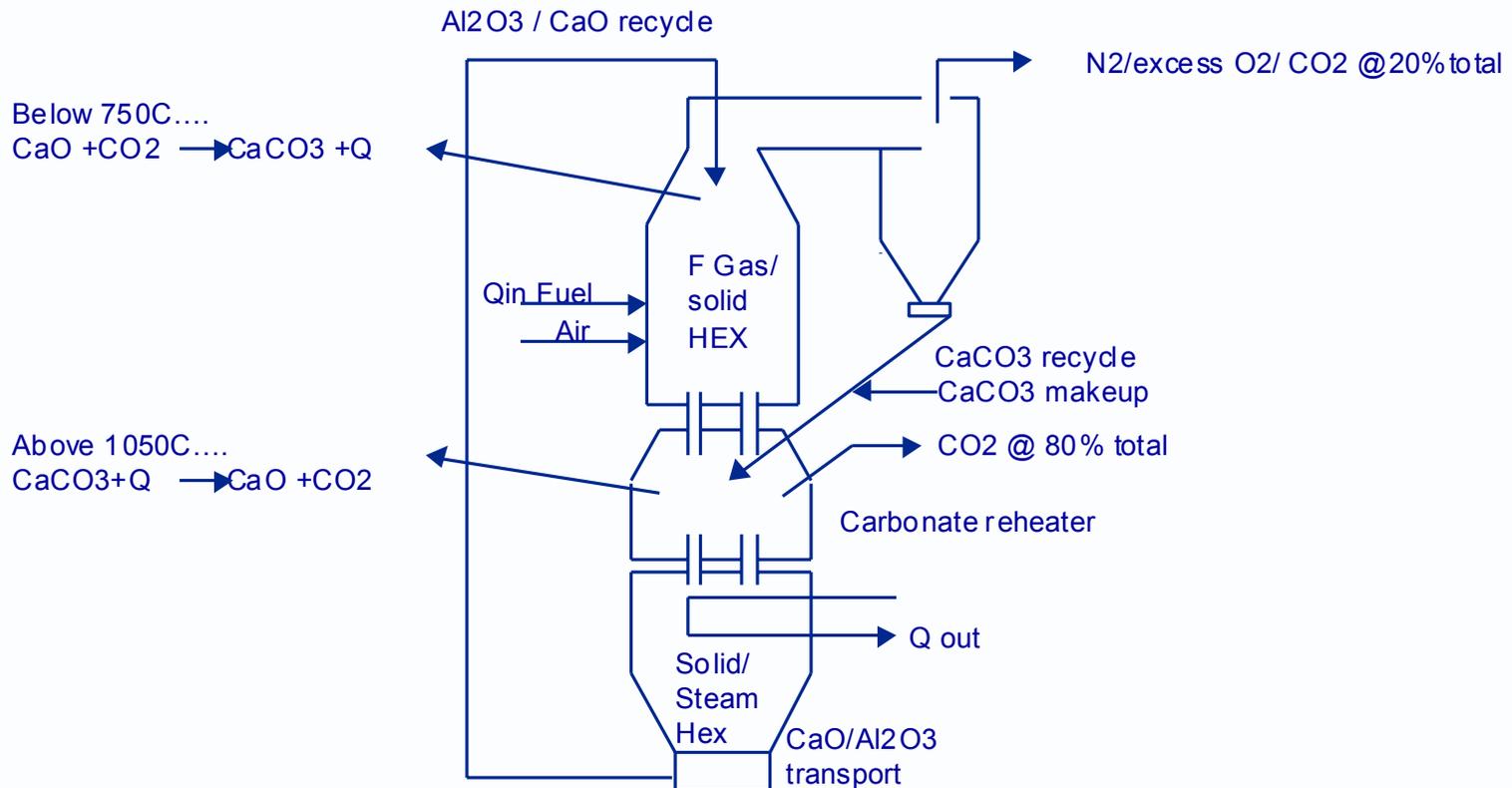
# Advanced Fluidized Bed



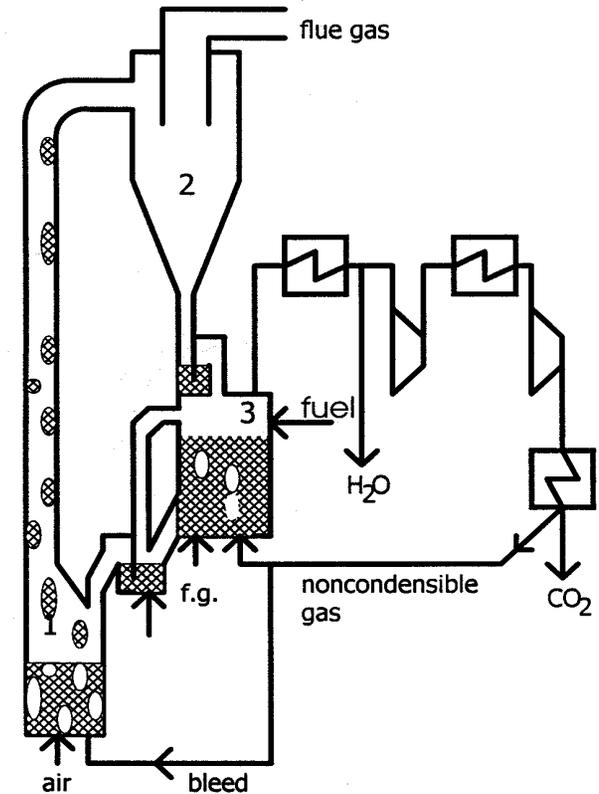
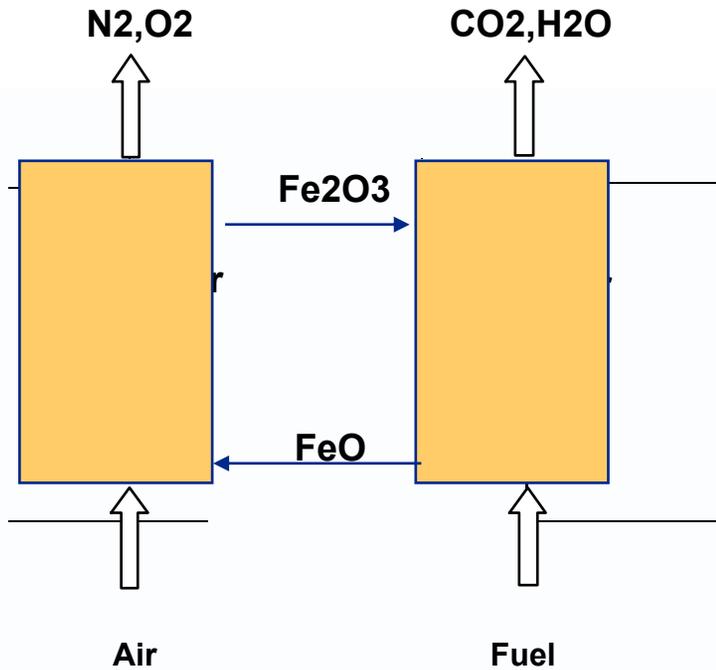
Power  
Technology



## CO2 capture via chemical looping



# Indirect Combustion

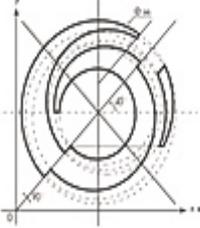


□ Atmospheric Pressure

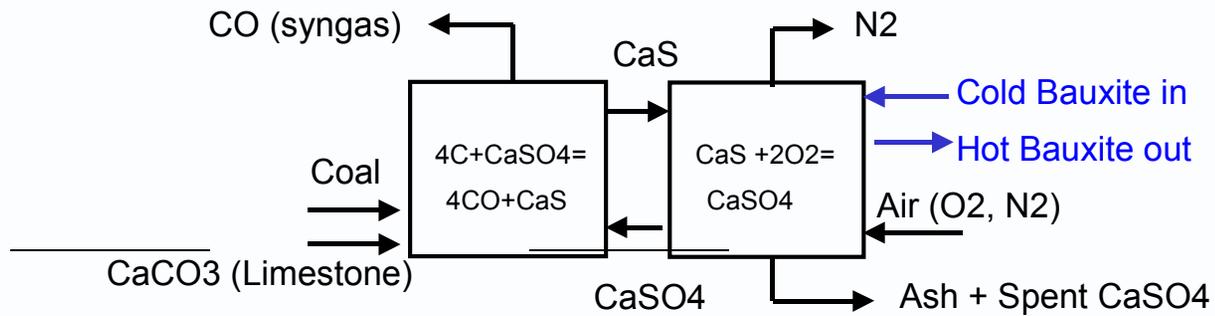
□ Oxygen carriers (Cu, Cd, Ni, Mn, Fe, Co)

□ Potential combustion process with interconnected FBC's

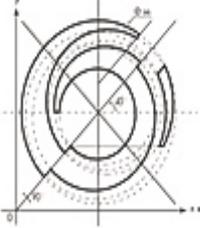
[ Ref. Lyngfelt & Leckner ]



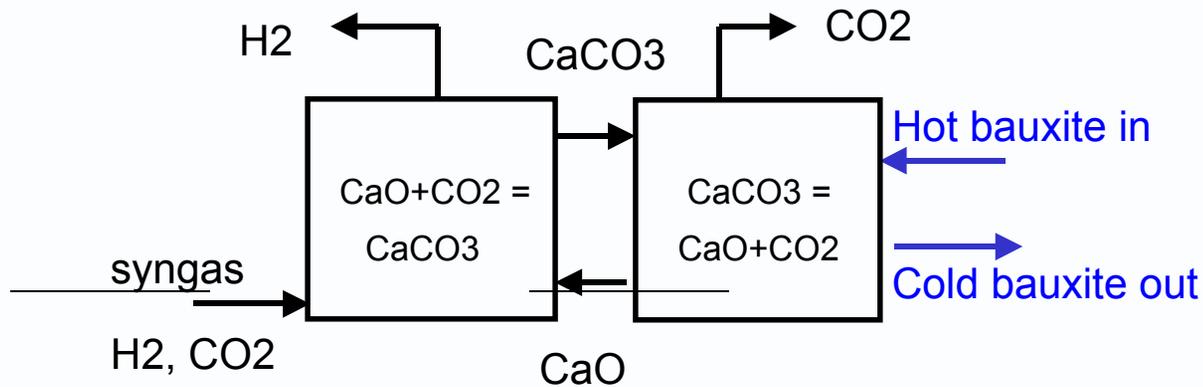
# Advanced Chemical Looping



[CaS to CaSO<sub>4</sub> chemical loop](#)



# Advanced Chemical Looping



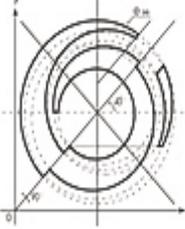
CaO to CaCO<sub>3</sub> Chemical loop

# Performance Comparison



	NGCC " H" class machine	Ultra supercritical PC	Thermie PC Normalized	IGCC cold gas clean-up H machine	Chemical looping H class cold clean	Chemical looping + SOFC
Cycle	Combined	Rankine	Rankine	combined	combined	SOFC+HRSG
Fuel	gas	coal	coal	coal	coal	coal
SH bar	124	345	375	125	123	165
SH C	565	649	700	538	568	538
1 stRH C	565	649	720	538	568	538
2 nd RH C		649	720			
GT inlet C	1427			1427	1427	
Aux pwr % gross	1.8	5.50	6.60	10.40	7.90	14.30
condensor bar	0.07	0.07	0.07	0.07	0.07	0.07
stack temp	86	146	138	132	135	130
HHV effcncy -no CO2	53.5	42.7	46.10	43.1	48.9	
LHV efficiency -no CO2	59.5	45.4	47.30	45.7	51.2	
kg of CO2/kwh no CO2	0.32	0.71	0.66	0.7	0.62	
HHV effcncy -with CO2	43.3	31.0	34.4	37.0	41.3	59.3
kg of CO2/kwh with CO2	0.044	0.104	0.091	0.086	0.077	0.054
source	EPRI Parsons	EPRI Parsons	Alstom normalized to Parsons	EPRI Parsons	preliminary Alstom Andrus	preliminary Alstom Andrus

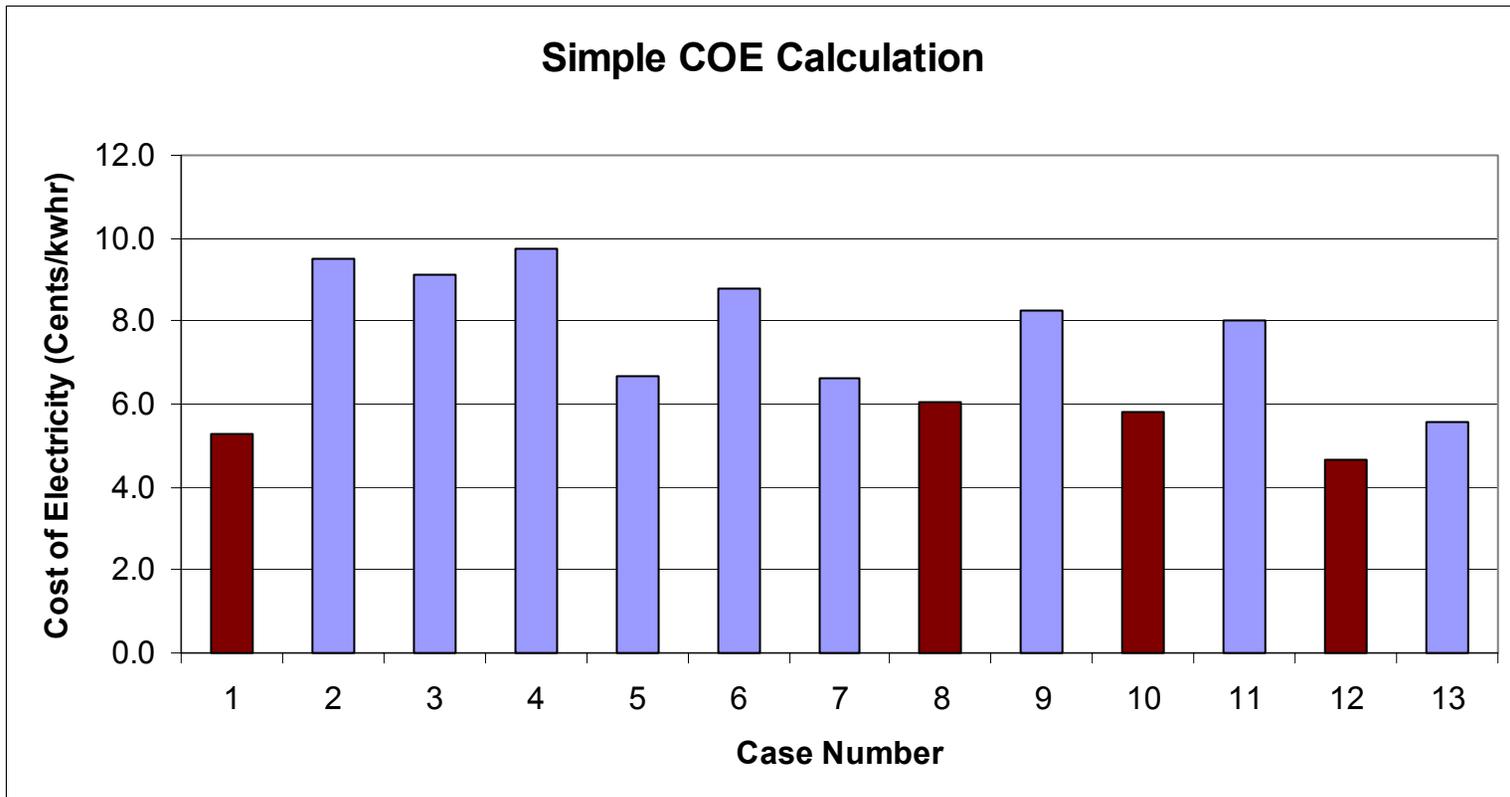
coal power is a real option

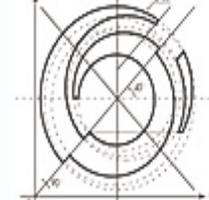


# Preliminary COE Comparison



- Advanced Chemical Looping Plants show promise for capturing CO<sub>2</sub>, meeting all other environmental requirements, improving efficiency, and being cost effective.





# CO2 Summary



Process	Technical Status	Cost	CO2 Reduction	CO2 Quality
Amine Scrubbing	Proven	Highest	90%	Food Grade
Oxygen Firing	Feasible	High (*)	100%	EOR
CO2 Wheel	New/Bench	Target (?)	50%	High
AFB/CO2	New/Paper	Target (?)	80%	High
Indirect Combustion	New/Bench	Moderate	90%	High
Chemical Looping	New/Bench	Moderate	90%	High
IGCC w/CO2	Proven	High	90%	Food Grade
Advanced Chemical Looping	New/Paper	Target	90%	High

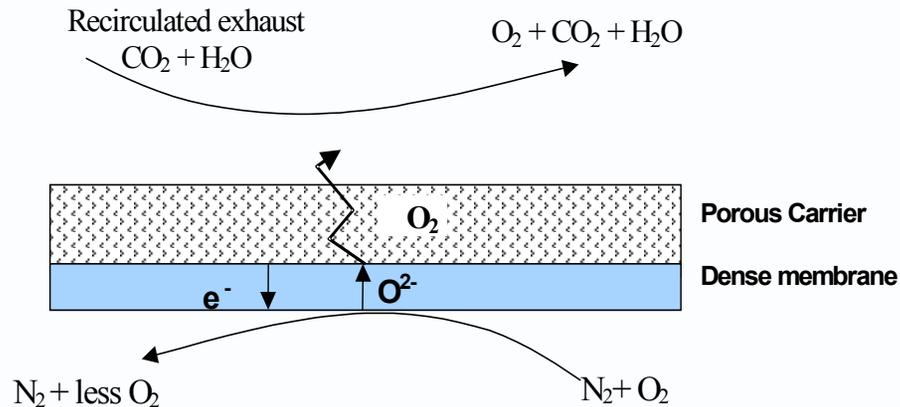
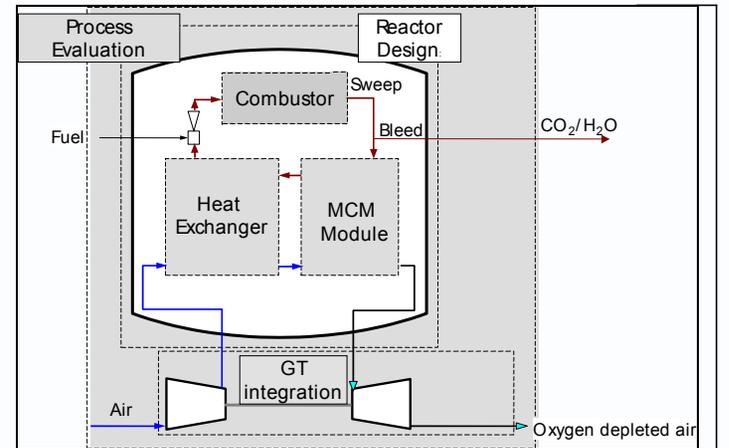
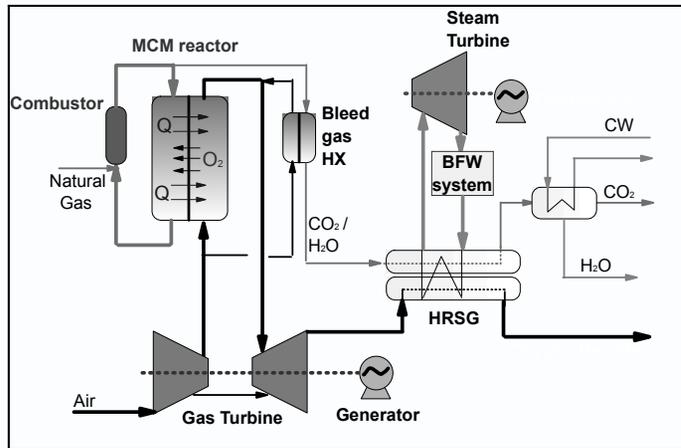
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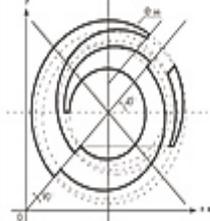


# Zero Emissions Gas Plant



- AZEP uses membrane technology to separate oxygen from air.



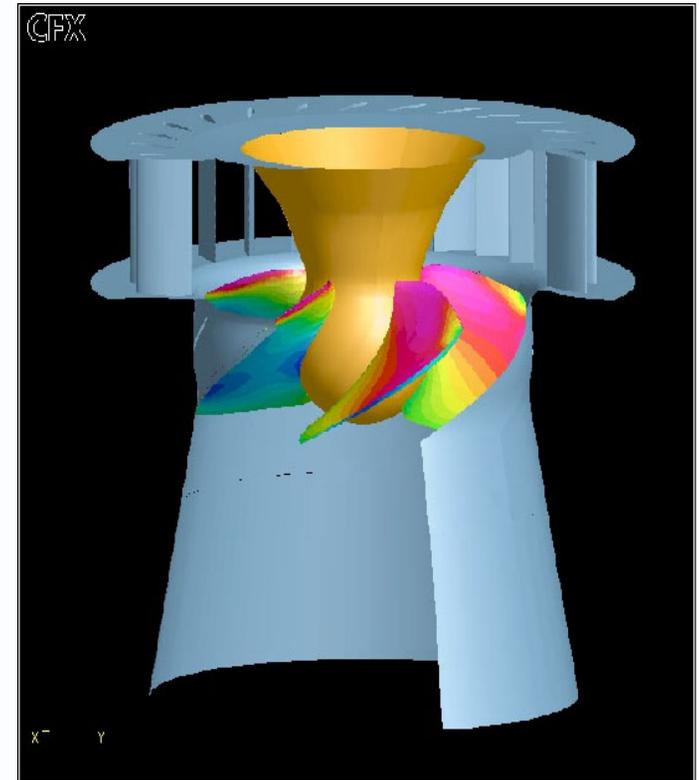


# Turbine Technology

ALSTOM

## New product : Green turbine

- Environment a real concern for ALSTOM :
  - Development of fish friendly turbine
  - Introduction of dissolving oxygen
  - Use of greaseless components
- Alstom active in industry groups addressing these issues:
  - DOE Advanced Hydro Power Turbine Program
  - Professional organizations like NHA R&D and Hydrovision



The Alstom logo features the word "ALSTOM" in a bold, sans-serif font. The letters "A", "L", "S", "T", and "M" are dark blue, while the "O" is red and stylized with three concentric, slightly offset circular segments. The logo is centered within a white semi-circular area that is bordered by a thick red arc on the left and top. The background consists of a blue gradient with abstract, curved lines.

**ALSTOM**

[www.alstom.com](http://www.alstom.com)